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IO WATER 5 COMMISSION ONTARIO WATER RESOURCES COMMISSION

Division of Plant Operations

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Water management in Ontario

Ontario Water Resources Commission

135 St. Clair Ave.W. Toronto 7 Ontario

We are pleased to present you with the Operating Summary for the water pollution control facilities operated for you during 1968.

Both the financial and technical information presented should be of assistance to your present and future planning in this important phase of municipal activity.

A new format has been devised to allow greater readability with equally detailed content. We trust that this will meet with your approval.

Our staff wish to express their appreciation for your co-operation throughout the year.

D. S. Caverly,

General Manager.

D. A. McTavish, P. Eng.,

Director.

Division of Plant Operations.

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135 St. Clair Avenue West

GEORGETOWN water pollution control plant

operated for

THE TOWN OF GEORGETOWN

by the

ONTARIO WATER RESOURCES COMMISSION

1968 ANNUAL OPERATING SUMMARY

FOREWORD

• This operating summary outlines the project's technical capabilities and financial status in 1968. Such information mirrors past and present performance, but a major intention is to anticipate the future -- to solve problems before they occur.

The new format in which this year's data are presented is designed to offer a higher level of readability than in the past, without a corresponding decrease in compactness, accuracy and detail.

Although your Regional Operations Engineer carries the major responsibility for the contents of the report, those involved in its preparation are attached to several Commission sections and divisions. The statistics section of the Division of Plant Operations compiled the information for the graphs and charts. The draughting section of the Division of Sanitary Engineering drew the graphs. The Division of Finance provided all cost data.

Only the close co-operation of these departments allowed the publication of this summary.

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768 REVIEW

The operating cost for the year was \$43,308.19, an increase of \$924.94 over 1967. The unit cost for treating one million gallons increased from \$65.19 in 1967 to \$80.29 in 1968.

In 1968 the plant treated an average flow of 1.47 mgd, which represents 98 percent of the design flow of 1.5 mgd. This design flow was exceeded 56 percent of the time during the year.

Reductions of 84 percent in BOD and 96 percent in suspended solids were experienced in 1968 in comparison to 87.1 percent in BOD and 89.7 percent in suspended solids in 1967. The average raw sewage strength was 84 mg/l for BOD and 250 mg/l for suspended solids. Raw sewage strength in 1967 was 85 mg/l for BOD and 233 mg/l for suspended solids.

The average final effluent BOD and suspended solids concentrations of 13 mg/l and 11 mg/l respectively were within the OWRC objectives.

PROJECT COSTS

NET CAPITAL COST	(Final)	2-0017-58	\$871,677.01	
DEDUCT payments f	rom Municipalities		48,379.33	
Long Tern	n Debt to OWRC			\$823, 297. 68
NET CAPITAL COST	(Final)	2-0077-61	\$ 63,230.31	
DEDUCT Portion Fin			19,072.10	
Long Terr	n Debt to OWRC			44, 158. 21
Total Long	\$ <u>867,455.89</u>			
Debt Retirement Bal (Sinking Fund) Decer	2-0017-58 2-0077-61	\$165,096.40 	\$ <u>171,670.88</u>	
	2-0017-58	2	2-0077-61	TOTAL
Net Operating	\$ 43,308.19	\$	50.07	\$ 43,358.26
Debt Retirement	16,614.00		891.00	17,505.00
Reserve	4,703.97		332.16	5,036.13
Interest Charged	46, 222. 76	2	,479.18	48,701.94
	\$110,848.76	\$3	,752.41	\$114,601.33

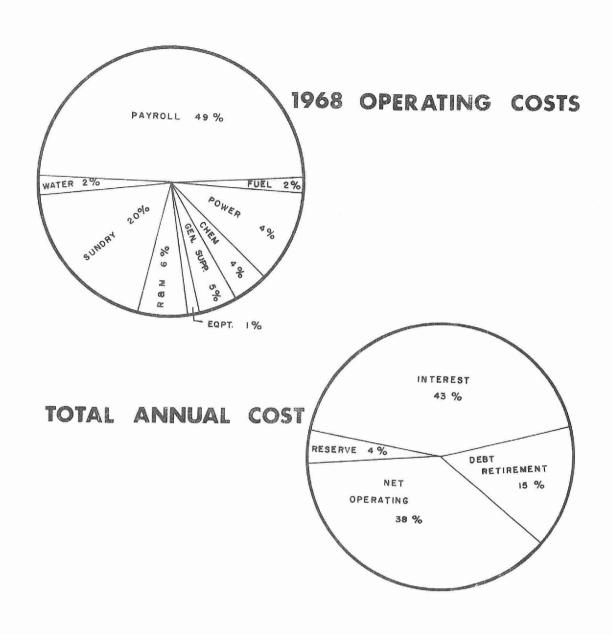
RESERVE ACCOUNT

	2-0017-58	2-0077-61	TOTALS
Balance @ Jan. 1, 1968	\$38,620.64	\$2,659.52	\$41,280.16
Deposited by Municipalities	4,703.97	332. 16	5,036.13
Interest Earned	2,297.28	164.71	2,461.99
	\$45,621.89	\$3,156.39	\$48,778.28
Less Expenditures	4,511.14		4, 511. 14
Balance @ Dec. 31, 1968	\$ <u>41,110.75</u>	\$3,156.39	\$ <u>44,267.14</u>

Monthly Operating Costs

MONTH	TOTAL EXPENDITURE	PAYROLL	CASUAL PAY ROLL	FUEL	POWER	CHEMICAL	GENERAL SUPPLIES	EQUIPMEŅT	REPAIRS &	* SUNDRY	WATER	TRAVEL
JAN	1526.56	1402.62	-	44.90	_		27, 75	_	25, 00	26, 29	-	55.72
FE8	2787.86	1392.73	_	159.93	448.81	238.61	176.74	-	277.86	37.46	_	57.40
MAR	3741.62	2217.84	187.07	91. 69	462,11	Teach)	66, 16	44.22	23. 52	591.61		95.48
APRIL	3421. 32	1400.85	-	90.94	439.55	238.61	167.13	-	338, 16	642.60	-	61.08
MAY	3714.11	1392.73	49.21	17.20	394.21	214.74	241.28	29.40	132.41	1181.05	- made	95.20
JUNE	4787.45	1408. 12	230.28	68. 62	412.33	238.61	320, 13	359.06	477.39	1177.71	=	80.08
JULY	2621.19	1378.22	312, 74	-	384.77	H	170.34	20.71	184.02	90.30	-	100.38
AIIG	5081, 99	1464.48	1134.23	-	329.67	238.61	208, 35	99.89	219,87	1286.51	-	100.00
SEPT	2225.76	983.85	286.55	-	350.25	238, 61	153.67	22.49	43. 23	47.11	=	27.15
ост	2560.05	991.17	311, 58	-	32, 33	_	106.09	26.00	304.47	761.26	-	95.55
NOV	4039.24	1413.66	142.94	-	631.49	238.61	140.78	-	88.29	1287.92	=	163.27
DEC	6801.05	2994.19	æ	255, 50	903.15	238, 61	282.69	25,00	503.80	1434.84	-	
TOTAL	43308.19	18448.4€	2654.60	728, 78	4788.67	1885.01	2061.11	626.77	2618.02	8564.66		932.11

^{*}SUNDRY INCLUDES SLUDGE HAULING COSTS WHICH WERE \$7,371.00



Yearly Operating Costs

YEAR M.G.TREATED		TOTAL COST	COST PER MILLION GALLONS	COST PER LB OF BOD REMOVED	
1964	307.12	\$29,738.15	\$ 96,82	10 cents	
1965	416, 54	31, 209, 58	90,76	11 cents	
1966	363.47	38, 306, 82	105.39	15 conts	
1967	650.11	42,383.25	65, 19	9 certs	
1968	539, 42	43,308.19	80. 29	11 cents	

Process Data

The average daily flow decreased from 1.75 mg in 1967 to 1.47 mg in 1968. The average design flow of 1.50 mgd was exceeded only 56 percent of the time during the year as compared to 90 percent of the time in 1967.

The average raw sewage BOD and suspended solids concentrations were respectively 84 mg/land 250 mg/l. The design BOD and suspended solids concentrations of 200 mg/l for each was exceeded only seven percent of the time for BOD and 20 percent of the time for suspended solids during the year.

The difference in the average concentrations of BOD and suspended solids in the raw sewage indicates a higher than normal ratio of inert to organic material. This is due to clay wastes from two paper mills.

The average final effluent BOD concentration of 13 mg/l and suspended solids concentration of 11 mg/l were within the OWRC objectives of 15 mg/l for each. The effluent BOD and suspended solids concentration in the final effluent exceeded the OWRC objective 34 percent and 13 percent of the time respectively during the year.

PLANT FLOWS and CHLORINATION

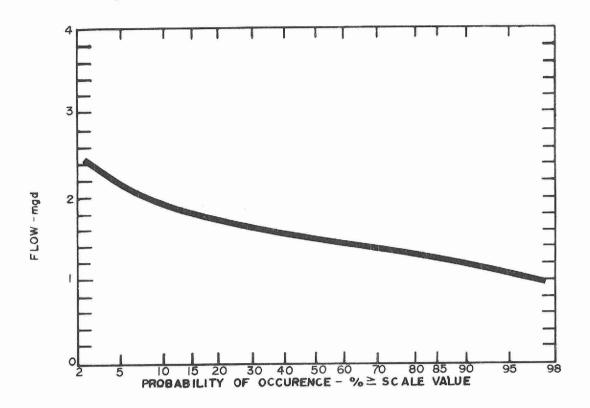
	TOTAL FLOW	AVERAGE	MAXIMUM DAILY FLOW	MINIMUM DAILY FLOW	CHLORINE USED	DOSAGE
MONTH	mg	DAILY FLOW	m g	m g	lbs.	mg/l
JAN	45, 95	1.48	2.28	1.31	806	1.9
FEB	51, 48	1.78	3.28	13. Š	984	1.9
MAR	60.50	1.95	2.61	1.46	1032	1, 7
APR	50.00	1.67	2.20	1.40	954	1.9
MAY	50.74	1.64	2.00	1.41	949	1.9
NUE	40.65	1.36	2.14	.85	1031	2, 5
JUL	* 33.14	1.07	1. 27	. 89	1207	3.6
AUG	41.02	1.32	1.90	. 80	1131	2.8
SEPT	41.07	1.37	2.04	1.20	1060	2.6
ост	39. 55	1.28	1, 86	1.07	1094	2.8
NOV	40.95	1.36	2, 24	. 85	. 1062	2.6
DEC	44.37	1.43	2.43	1.07	1129	2.5
TOTAL	539.42	344	_		12439	_
AVERAGE	_	1.47	_	_	1037	2.3

^{*} Prorated on 21 days data

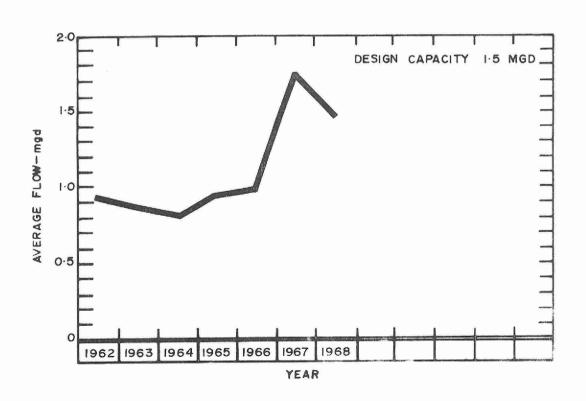
COMMENTS

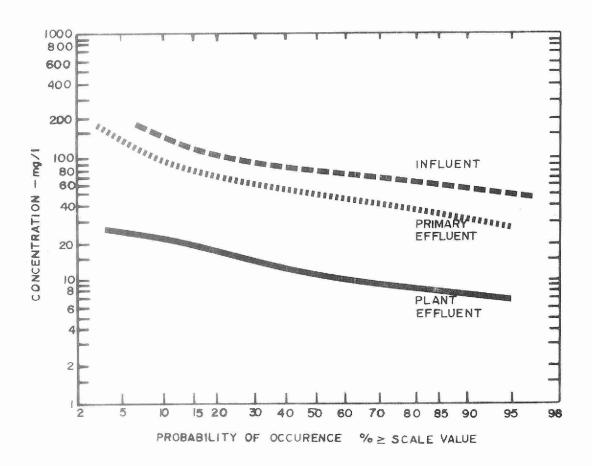
A total of 1,037 lbs. of chlorine at an average dosage rate of 2.3 mg/l was required to maintain a chlorine residual of 0.5 mg/l in the final effluent.

The flow meter was repaired after readings approximately 25% low were obtained prior to the fall of 1967. Steps have been taken to provide separated sewers, resulting in a decrease in total flows in 1968.

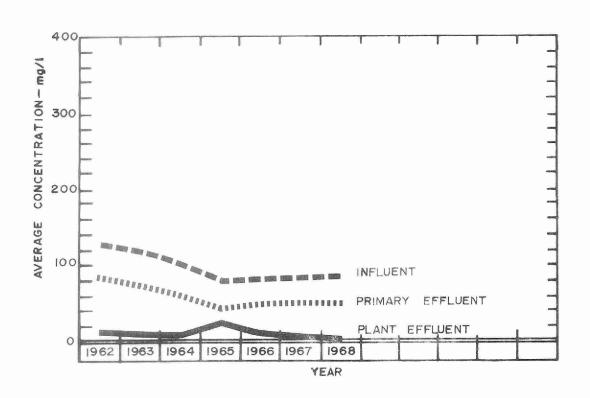


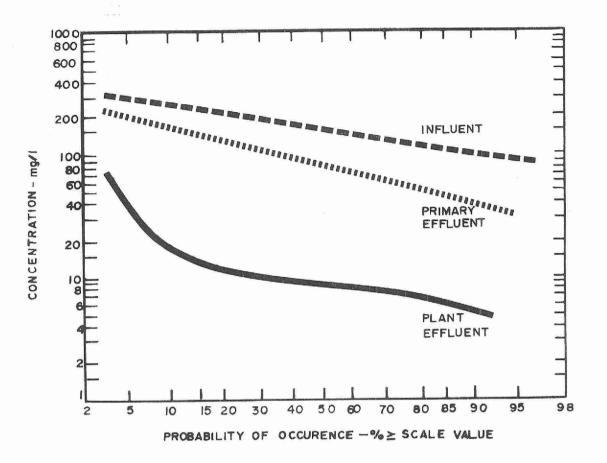
FLOWS



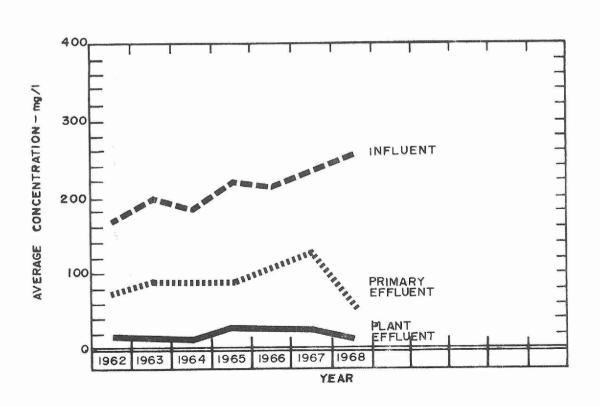


BIOCHEMICAL OXYGEN DEMAND





SUSPENDED SOLIDS



PLANT EFFICIENCY

	8100	HEMICAL	OXYGE	N DEMAND		SUSPE	NDED SO	oL(DS	GRIT
MONTH	INF CONC ^N mg/I	EFF CONC ^N mg/l	RED [™] %	REMOVAL 10 ³ 16	INF CONC ^N mg/l	EFF CONC ^N mg/l	RED ^N	REMOVAL 10 ³ 1b	REMOVAL
NAL	77	22	71	25.3	189	13	93	80.9	25
FEB	93	20	78	37.5	171	15	91	80.3	45
MAR	101	20	80	49.0	141	8	94	80.5	17
APR	109	9	92	50.0	112	5	96	53 . 5	14
MAY	105	10	90	48.2	199	5	98	98.4	27
MUL	74	9	88	26.4	130	5	96	50.8	26
JULY	68	8	88	19.8	167	7	96	53.0	20
AUG	48	9	81	16.0	63	6	66	23.4	59
SEPT	76	11	86	26.7	137	40	71	39.8	12
ост	65	8	88	22.7	177	5	97	68.0	_
NOV	123	14	89	44.6	134	5	96	52.8	54
DEC	66	10	85	24.8	104	11	89	41, 3	6
TOTAL	-	April 1	-	391.1	-	-		722.7	-
AVERAGE	84	13	84	32.5	250	11	96	60.2	28

COMMENTS

Plant efficiency improved from 1967 to 1968 with respect to suspended solids reductions. The average final effluent suspended solids concentration was reduced from 23 mg/l in 1967 to 11 mg/l in 1968. The overall average suspended solids reduction increased from 89.7 percent to 96 percent.

The BOD reductions were similar to the reductions experienced in the previous year.

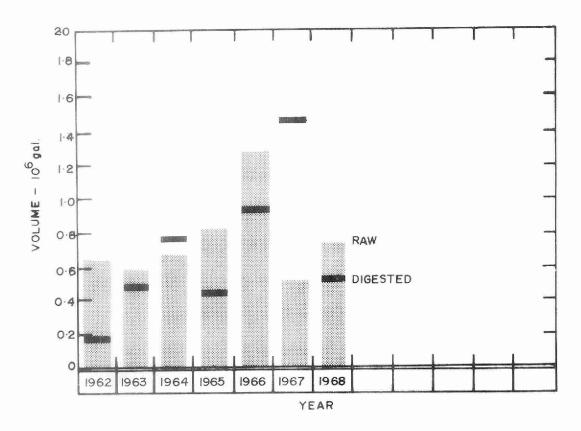
AERATION

		PRIMARY EFF		SECON	DARY EFF			*	
MONTH	AVERAGE FLOW mgd	BOD CONC ^M mg/l	SS CONC ^N mg/I	BOO CONC ^N mg/l	SS conc™ mg/l	MLSS CONC ^N mg/l	F/M (16 BOD 16MLSS)	(1000 ft) IN BOD REMOVED	WASTE SLUDGE Ib
JAN	1.48	67	111	22	13	1,890	. 12	-	-
FEB	1.78	101	150	20	15	1,840	. 18	-	
MAR	1.95	77	90	20	8	1,440	. 20	***	-
APRIL	1.67	61	64	9	5	1,540	. 26	-	
MAY	1.64	62	124	10	5	1,270	. 15	<u></u>	-
JUN	1.36	26	34	9	5	1 330	. 05) page.	-
JUL	1.07	35	61	8	7	1, 140	.06	_	=
AUG	1.32	48	68	9	6	2,550	. 05	_	Sind
SEPT	1.37	36	65	11	40	2,070	. 04	-	
ост	1.28	32	56	8	5	1,340	.05	_	-
NOV	1.36	78	49	14	5	1,340	. 15	-	-
DEC	1.43	26	40	10	11	1,750	. 04	_	-
TOTAL	-	-	-	-	-	=		-	×
AVE R A GE	1.47	54	76	12	1.0	1,625	. 11	_	_

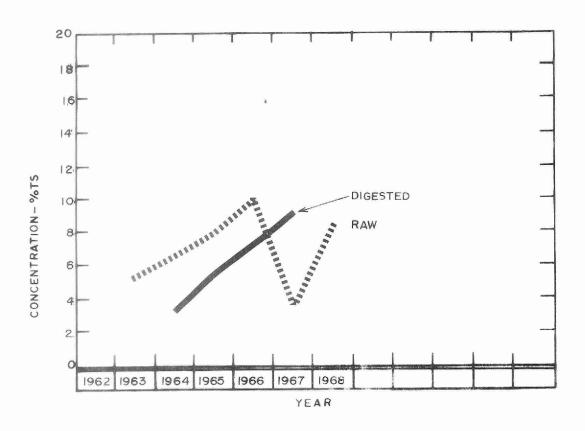
^{*} mechanical aeration

COMMENTS

The average loading on the aeration section was similar to the loading experienced in the previous year at 0.11 lbs. of BOD per lb. of MLSS. Excellent treatment was obtained at this loading throughout the year.



DIGESTION



SLUDGE DIGESTION and DISPOSAL

	RAW	SLUDGE		DIGES	TED SL	JDGE	SUPERN	ATANT	SLUDGE	DISPOSAL
MONTH	VOLUME 1000 gai	T.S. %	∨.5. %	VOLUME 10 ⁵ gal	T. S.	V.S. %	VOLUME gai	T. S. %	LIQUID yd ³	DEWATERED yd3
JAN	-	-	-	0	-	-	-	-	0	0
FEB	-	_	-	0	-	-	_	-	477	0
MAR	-	11.7	48	0	-	-	-	-	612	0
APR	-	6.0	61	0	-	-	-	1	1080	0
MAY	-	7.7	62	1.87	+	_	-	-	1107	0
JUN	-	6.4	55	. 97		-	-	-	576	0
JUL	-	-	-	1.06	-	-	-	-	630	0
AUG	-	Same	-	1.20	-	2		-	711	0
SEPT	-	_	-	0	-		=	-	522	0
ост	-	7.8	54	0	-	-	-	_	720	0
NOV	-	7.0	44	0	-		-	1	621	0
DEC	-	10.0	55	0	-	-	jan-		369	0
TOTAL	* 660	=	-	5, 10	1000	_			7.125	0
AVERAGE	_	8.1	54	0	-	_	_	ment)	675	0

^{*}Estimated

COMMENTS

Because of problems with the operation of the digester, sludge digestion was carried out only for four months of the year. During the other months, raw sludge was hauled directly from the primary tanks.

A heavy sludge in the digester, consisting mostly of clay wastes, prohibited effective digester operation. An attempt to empty the digester during the summer was unsuccessful as the pump was incapable of handling the heavy sludge. A new pump has been ordered to overcome this situation.

Date Due

-	 	

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CONCLUSIONS

An average flow of 1.47 mgd was treated at the plant during the year. This represented a flow equal to 98 percent of the plant design capacity.

The average final effluent, BOD and suspended solids concentrations of 13 mg/l and 11 mg/l respectively were within the OWRC objectives of 15 mg/l for each.

RECOMMENDATIONS

Expansion should be initiated in the near future.



Water management in Ontario